IN THE CLAIMS

Please amend the claims as follows:

Claim 1 (Currently amended): A method of preparing 1,3-dichloro-2-propanol and 2,3-dichloro-1-propanol comprising hydrochlorinating glycerine ~~and/or monochloropropanediols~~ with gaseous hydrogen chloride with catalysis of a carboxylic acid, wherein said hydrochlorination is carried out solvent-free in at least one continuous reaction zone at reaction temperatures in the range of 70-140°C and with continuous removing of the water of reaction by distillation at reduced pressure, [[the]] a liquid feed containing at least 50% by weight of glycerine ~~and/or monochloropropanediols~~.

Claim 2 (Currently amended): The method according to claim 1, wherein the liquid feed contains 80-100% by weight of glycerine.

Claim 3 (Currently amended): The method according to claim [[1]] 17, wherein said monochloropropanediol is ~~the liquid feed contains, as the monochloropropanediol,~~ 3-chloro-1,2-propanediol ~~and/or 2-chloro-1,3-propanediol~~.

Claim 4 (Previously presented): The method according to claim 1, wherein the catalysis is made with acetic acid.

Claim 5 (Previously presented): The method according to claim 1, wherein the reaction is carried out at a temperature of 100-110°C.

Claim 6 (Previously presented): The method according to claim 1, wherein the distillation at reduced pressure is carried out in a rectification zone linked to the reaction

zone.

Claim 7 (Previously presented): The method according to claim 6, wherein the method comprises removing of the water of reaction by distillation and at least partial primary collection of the 1,3-dichloro-2-propanol and 2,3-dichloro-1-propanol product.

Claim 8 (Previously presented): The method according to claim 7, wherein secondary collection is made, from which dichloropropanols and monochloropropanediols are recycled to the process.

Claim 9 (Previously presented): The method according to claim 8, wherein the secondarily collected residual balance of the reaction mixture is subjected to distillation under reduced pressure in order to separate the higher boiling waste products as the distillation residue and the dichloropropanols and monochloropropanediols, recycled to the reactor, as the distillate.

Claim 10 (Previously presented): The method according to claim 1, wherein the method is carried out in a cascade of continuous flow reaction zones wherein the water of reaction is collected, together with partial collection of the product dichloropropanols, by distillation at reduced pressure, located always downstream the individual reaction zones of the cascade, and the distillation residue is fed into the next zone of the cascade.

Claim 11 (Previously presented): The method according to claim 10, wherein the reaction mixture exiting from the last step of the cascade is subjected to a two-step distillation, wherein in the first step the water of reaction is separated together with the

dichloropropanol reaction product as the distillate and in the second step the higher boiling waste products are separated as the distillation residue and the dichloropropanols and monochloropropanediols are separated as the distillate and are recycled back to the process, preferably into the first step of the cascade.

Claims 12-16 (Canceled).

Claim 17 (New): A method of preparing 1,3-dichloro-2-propanol and 2,3-dichloro-1-propanol comprising hydrochlorinating monochloropropanediols with gaseous hydrogen chloride with catalysis of a carboxylic acid, wherein said hydrochlorination is carried out solvent-free in at least one continuous reaction zone at reaction temperatures in the range of 70-140°C and with continuous removing of the water of reaction by distillation at reduced pressure, a liquid feed containing at least 50% by weight of monochloropropanediol.

Claim 18 (New): The method according to claim 17, wherein said monochloropropanediol is 2-chloro-1,3-propanediol.

Claim 19 (New): The method according to claim 17, wherein the catalysis is made with acetic acid.

Claim 20 (New): The method according to claim 17, wherein the reaction is carried out at a temperature of 100-110°C.

Claim 21 (New): The method according to claim 17, wherein the distillation at reduced pressure is carried out in a rectification zone linked to the reaction zone.

Claim 22 (New): The method according to claim 21, wherein the method comprises removing of the water of reaction by distillation and at least partial primary collection of the 1,3-dichloro-2-propanol and 2,3-dichloro-1-propanol product.

Claim 23 (New): The method according to claim 22, wherein secondary collection is made, from which dichloropropanols and monochloropropanediols are recycled to the process.

Claim 24 (New): The method according to claim 23, wherein the secondarily collected residual balance of the reaction mixture is subjected to distillation under reduced pressure in order to separate the higher boiling waste products as the distillation residue and the dichloropropanols and monochloropropanediols, recycled to the reactor, as the distillate.

Claim 25 (New): The method according to claim 17, wherein the method is carried out in a cascade of continuous flow reaction zones wherein the water of reaction is collected, together with partial collection of the product dichloropropanols, by distillation at reduced pressure, located always downstream the individual reaction zones of the cascade, and the distillation residue is fed into the next zone of the cascade.

Claim 26 (New): The method according to claim 25, wherein the reaction mixture exiting from the last step of the cascade is subjected to a two-step distillation, wherein in the first step the water of reaction is separated together with the dichloropropanol reaction product as the distillate and in the second step the higher boiling waste products are separated as the distillation residue and the dichloropropanols and monochloropropanediols are

separated as the distillate and are recycled back to the process, preferably into the first step of the cascade.